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ADVANCE
ENVIRONMENTAL

AGGREGATE INDUSTRIES UK LIMITED
DOYLE DRIVE
COVENTRY
WEST MIDLANDS

Environmental Protection Act
Pollution Prevention & Control

PARTICULATE EMISSION TEST
(BS EN 13284-1:2017)

on

ROADSTONE COATING PLANT
BAG FILTER EXHAUST

for

AGGREGATE INDUSTRIES UK LIMITED
DOYLE DRIVE
COVENTRY
WEST MIDLANDS
CV6 6NW

Report Prepared by:

K Gough Company Principal	A Yelland Associate	Date Of Test : 10.12.19 Date Of Report : 19.12.19 Report No : 3183 EPR No :

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EXECUTIVE SUMMARY

EMISSIONS SUMMARY

Determined	**Units**	**Results**	**Uncertainty** +/-	**Limit**
Particulate Concentration (STP)	mg/Nm^3	35.4	1.05	50
Mass Emission (STP)	Kg/hr	0.92	0.03	-
Stack Temperature	°C	77	-	-
Gas Velocity	m/s	15.48	-	-
Stack Volume Flow Rate (Actual)	m^3/hr	35449	-	-
Stack Volume Flow Rate (STP)	m^3/hr	27124	-	-

All results are reported at reference conditions of 273K, 101.3kPa, wet gas.

MONITORING TIMES

Determined	**Sampling Date**	**Sampling Times**	**Sampling Duration**
Total Particulate Matter Run 1	10.12.19	07.24 - 07.56	32 minutes
Total Particulate Matter Run 2	10.12.19	08.02 - 08.34	32 minutes
Preliminary Stack Traverse	10.12.19	07.20	-

PROCESS DETAILS

Determined	**Process Details**
Process description	ROADSTONE COATING PLANT
Continuous or Batch	Continuous - various grades @ 40tph.
Particulate type	Aggregate
Abatement	Bag Filter
Appearance of plume	Steam

MONITORING METHODS

Determined	**Method**	**Technical Procedure**	**Limit of Detection**	**Calculated MU +/-%**
TPM	BS EN 13284-1	EL18	0.08	8.0%
Velocity	BS EN ISO 16911-1	EL20	-	-
Volumetric Flow	BS EN ISO 16911-1	EL20	-	-

1. BACKGROUND INFORMATION

Particulate emission testing was undertaken by Advance Environmental Consulting Limited, on the roadstone coating plant bag filter exhaust at Aggregate Industries UK Limited, Coventry site.

The purpose of the emission testing was to ensure compliance with the requirements of the permit issued by the Local Authority under The Environmental Permitting (England and Wales) Regulations 2010.

2. MONITORING PROTOCOL

2.1 Test Method and references

Isokinetic sampling of the contained emission sources was undertaken using the APEX Instruments Inc Method Five isokinetic sampling apparatus in accordance with the main procedural requirements within the following British Standards and Technical Guidance Notes:-

* BS EN 13284-1:2017 - Stationary source emissions. Determination of low range mass concentration of dust.

* Environment Agency - Technical Guidance Document (Monitoring) M1 Sampling requirements for monitoring stack emissions to air from industrial installations; and

* Environment Agency - Technical Guidance Document (Monitoring) M2 Monitoring of Stack Emissions to Air.

2.2 Sampling procedure

The work carried out was, as far as was reasonably practical, in accordance with BS EN 13284-1:2017.

Isokinetic flow means that sample gases laden with particulates are drawn off at the same velocity as the free stream velocity in the flue. Isokinetic sampling thus avoids possible inertial effects of particulates approaching the vicinity of the inlet nozzle which may result in significant

The Apex Instruments test equipment was designed to meet the sampling requirements of US EPA Method 5 and with a modified nozzle design, meets the sampling requirements of BS EN 13284-1.

The principle of the standard is to draw a known volume of dust laden gas isokinetically through a filter. The weight gain on the filter, after sampling, divided by the gas sample volume equates to the particulate concentration, which in turn can be used to calculate a mass emission.

2.3 Sampling equipment

The test equipment is inspected prior to use and it's calibration status observed. This includes:-

* *Pitot Tube* - All pitot tubes are checked for damage, alignment and that there are no blockages;

* *Manometer* - Check of oil levels, connectors and orientation level

* *Thermocouple* - Temperature is measured using k type thermocouples. Each thermocouple is inspected for calibration and damage. Digital temperature meters are used in conjunction with k type thermocouples which are also checked for calibration dates;

* *Gas meter* - The calibration of the gas meter is checked before and after sampling using a critical orifice.

* *Nozzles* - All nozzles used have been constructed in accordance with BS EN 13284-1. Each nozzle is checked for damaged and measured using a Vernier calliper on at least 3 planes. Non conforming nozzles will be rejected.

* *Balance* - A Mettler Toledo balance is used to weigh filters. It is calibrated yearly by the manufacturer and checked daily by in-house weights.

* *Filters* - Quartz membrane filters with a collection efficiency of >99.5% at 0.3microns

2.4 Preparation for sampling

2.4.1 Filter preparation

Filters are pre-conditioned before arrival on site. The filters are dried in an oven at 180°C for a period of at least one hour and then placed to cool in a desiccator for at least four hours. The filters are then weighed on a five figure balance and placed in individual transport containers. Spare Filters are prepared to obtain blank values.

2.4.2 Sampling location

No site visit was undertaken prior to undertaking the sampling procedure, as monitoring had previously been undertaken at the site, during which time the sampling position, working platform, sampling ports, access and safety precautions were found to be satisfactory.

The internal dimension of the flue was known from previous monitoring undertaken. However, further measurements were taken to check that the internal diameter had not changed.

Prior to sampling a pressure and temperature survey, using a pitot static tube, a micromanometer, a digital thermometer and a nickel-chromium/nickel-aluminium thermocouple, is carried out to check whether the flow conditions meet with the requirements of BS EN 16911. From this initial survey sample locations, isokinetic flow rates, nozzle size, and sample period can be worked out.

2.5 Sample collection

A leak check is carried out before and after sampling to confirm all the suction is drawn through the nozzle.

With the required isokinetic flow rates known the sample probe is inserted into the stack at 90° to the gas flow, this is to stop any particulate matter impinging on the filter before sampling.

The filter head and probe were allowed to obtain the stack gas temperature.

The initial gas meter reading was noted and the suction device and timer started. The correct flow rate for isokinetic sampling was set and the nozzle positioned to face parallel to the gas

Sampling was then carried out for the planned duration and number of sample points, recording all the necessary data for final calculations. On completion, the suction device and timer were stopped and the final gas meter volume recorded.

The probe was removed from the process stack and a further leak test carried out prior to removal of the filter, which was subsequently removed and placed in a storage container.

Any residual particulates upstream of the filter was washed with acetone into an appropriate beaker.*In stack filter used no requirement for washing.

Repeat all of the above procedures to obtain duplicate samples.

At all times during the sampling procedure the sampling technicians were in contact with the process operator to ensure that the plant was in full production and there were no changes in the process that might affect the representative nature of the samples collected.

2.6 Analysis of samples

On returning to the laboratory, the used filters were dried in an oven at 160°C for a minimum of one hour and then desiccated and weighed as before. The water/acetone washings are first evaporated, without boiling, then dried and weighed as above. The total particulate mass is the sum of the differential filter weight added to the differential water/acetone rinsing's component.

2.7 Calculation of results

The calculations were made using the formula specified in BS EN 13284-1.

The recorded filter weights, velocity, temperature, sampling duration and internal flue dimensions were then used to calculate:-

* the mass rate of solids emission in kg/hr; and
* the solids concentration in mg/m^3.

2.8 Comments

On the completion of sampling, the data from the PCME DT990 continuous emission monitor was interrogated and the average results, which were recorded during the measurement period, noted. A level of 40.3289mg/m3 was obtained together with an existing calibration factor of 1.3255. It can be concluded that the monitor would benefit from an adjustment of the current calibration factor to 1.1635.

3. QUALITY ASSURANCE

3.1 Location

SAMPLING LOCATION					
Determined	**Value**	**Units**	**Requirement**	**Compliant**	**Method**
Lowest differential pressure	105	Pa	>= 5Pa	Yes	BS EN 15259
Highest differential pressure	130	Pa	-	-	
Ratio of gas pressures	1.2	Pa	<9:1	Yes	BS EN 15259
Mean gas velocity	15.5	m/s	-	-	-
Temperature deviation	3	K	<10%	Yes	BS EN 13284
Max angle of flow	<15	o	<15°	Yes	BS EN 15259
No local negative flow	Yes	-	-	Yes	BS EN 15259

Duct Details		
	Value	Units
Shape	Circular	-
Depth	0.90	m
Width		m
Area	0.64	m^2
Port	0.09	m

Duct Details	
	Isokinetic
Sample port size	4" BSP
Number of lines used	2
Number of points/line	2
Duct orientation	Vertical
Filtration for TPM	In stack

3.2 Methods

MONITORING METHODS		
Determined	**Method**	**Technical Procedure**
TPM	Gravimetric	EL18
H2O	Gravimetric	EL5

3.3 Test Team

MONITORING TEAM						
Personnel	**MCERTS**	**MCERTS**		**TE/H&S Qualifications**		
	Number	**Level**	**Expiry**	**TE1**	**H&S**	
Andrew Yelland	MM 02 130	MCERTS Level 2	Apr-23	Apr-23	Jul-24	

4. ON-SITE SUMMARY/MEASURMENTS

TOTAL PARTICULATE MATTER SUMMARY				
Determined	**Sampling Times**	**Concentration mg/m^3**	**Uncertainty mg/m^3**	**Limit mg/m^3**
Run 1	07.24 - 07.56	37.61	1.05	50
Run 2	08.02 - 08.34	33.17	0.93	50
Blank	-	0.08	-	-

FILTER SUMMARY					
Determined	**Filter No**	**Filter Start Weight g**	**Filter Start Weight g**	**Acetone Rinse Weight g**	**Combined Mass Gained g**
Run 1	25	0.05597	0.07985		0.02388
Run 2	26	0.05609	0.07664		0.02055
Blank	27	0.05586	0.05591		0.00005

STANDARD UNCERTAINTY SUMMARY								
Measured Quantities	**Value**	**Standard uncertainty**			**Uncertainty %**	**Requirement of std**		
Sampled Volume - V_m	0.7151	uV_m	0.001	**m^3**	0.14		<=2%	Pass
Sampled gas Temp - T_m	279	uTm	2	k	0.72		<=1%	Pass
Sampled gas Pressure - ρm	99.5	$u\rho_m$	0.5	**kPa**	0.50		<=1%	Pass
Sampled gas Humidity - Hm	4.74	uH_m	1	**% by vol**	0.21		<=1%	Pass
Oxygen content - O2,m	17.9	$uO_{2,m}$	0.1	**% by vol**	0.56		<=5%	Pass
Mass particulate - m	23.88	um	0.01	**mg**	0.04	0.03	<5% of limit val	
Note - Sampled gas humidity, temperature and pressure are values at the gas meter								Pass
Leak - L	0.34			**%**	0.34		<=2%	Pass
Uncollected Mass - UCM (In stack filter - no rinse)	0.05			**mg**	0.21		<=10%	Pass

MOISTURE SUMMARY					
RUN	**Trap Start Weight g**	**Trap End Weight g**	**Difference g**	**Volume sampled m^3**	**Bwo %**
Run 1	538.3	563.8	25.5	0.6349	4.74
Run 2	540.5	566.4	25.9	0.6196	4.93

4.1 Preliminary stack survey

On Site Velocity and Flow Data

Company	AGGREGATE INDUSTRIES UK LIMIT	Stack Diameter	0.90	m
Site	DOYLE DRIVE	Area	0.64	m^2
Location	ROADSTONE COATING PLANT	Sample points required	4	
Job No	3183	Barometric Pressure	99.5	kPa
Operators	AJY	Stack Pressure	0.01	kPa
		Pitot Tube Coefficient	0.997	

Preliminary readings taken before sampling				
	Pitot Traverse A		Pitot Traverse B	
Pitot Settings	D P pa	Temp °C	D P pa	Temp °C
1	105	77	108	76
2	117	78	119	76
3	119	78	123	77
4	122	78	125	77
5	124	78	128	77
6	127	79	130	77
7	125	79	128	77
8	122	78	126	78
9	119	78	123	77
10	108	78	115	77
Mean	119	78	123	77

4.2 Leak check results

PITOT LEAK CHECK

Run	Pre traverse leak rate			Post traverse leak rate		
	Start value Pa	End value Pa	Difference %	Start value Pa	End value Pa	Difference %
Run 1	250	250	Pass	250	250	Pass
Run 2	250	250	Pass	250	250	Pass

S-TYPE STAGNATION CHECK

Run	Stagnation Pa	Reference Pa	Difference Permitted +/- 10 Pa
Run 1	45	45	Pass
Run 2	45	45	Pass

SAMPLE TRAIN LEAK CHECK

Run	Mean Sampling Rate litres/min	Pre-sampling Leak Rate litres/min	Post-sampling Leak Rate litres/min	Acceptable Leak Rate litres/min	Maximum Leak Rate %
Run 1	26.47	0.09	0.09	0.53	Yes
Run 2	26.16	0.10	0.10	0.52	Yes

SAMPLE TRAIN LEAK CHECK

Run	Blank Value mg/m^3	Emission Limit Value mg/m^3	Acceptable Blank Value mg/m^3	Blank Value Acceptable mg/m^3
Blank 1	0.08	50	5	Yes

5. SAMPLING RECORDS

5.1 Process Conditions

Arrestment Plant:	Bag Filter
Particulate Type:	Aggregate
Plant Loading:	Continuous - various grades @ 40tph.
Appearance of plume:	Steam

5.2 Sampling Results

	Test Run No. 1.	Test Run No. 2.	Average
Time of Test:	07.24 - 07.56	08.02 - 08.34	
Sampling Duration: (mins)	32	32	
Gas Temperature (°C)	77	76	77
Mean Velocity at Sampling Points: (m/s)	15.61	15.42	15.51
Gas Flow Rate at STP (1): (m^3/min)	434.5	430.0	432.2
Particulate Loading at STP (1): (mg/m^3)	37.61	33.17	35.39
Particulate at Normalised Conditions (2): (mg/m^3)	-----	-----	-----

(1) Particulate stated at 273K, 101.3kPa without correction for water vapour.

(2) State normalised conditions (e.g. 11% O_2, etc).

5.3 - Calculations Sample Run No. 1

On-site measurements

O2 = 17.9 % CO2 = 1.7 % N2 = 80.4 %
Bws = 0.05 Ps = 99.5 kPa Ts = 350.3 K

Md = Molecular weight of gas at DGM (g/g mole)
Md = (0.44 x %CO_2) + (0.32 x %O_2) + (0.28 x %N_2)
= 28.99 g/g mole

Ms = Molecular weight of gas wet (g/g mole)
= 28.44 g/g mole

Stack gas velocity at sample points

V = Kp x Cp x Ö(Ts.DP/Ps.Ms)
= 15.61 m/s

Kp = 4.07
DP = 119.5 av. Dp at sample plane
Cp = 1.00 pitot tube coefficient

Stack gas volume at sample points

Q = V x A x 60
= 595.7 m^3/min

A = 0.64 area of stack m^2

Volume of water vapour collected, standard conditions (m^3)

Vwstd = 0.00124 x Vlc
= 0.0316 m^3

Vlc = 26 ml

Volume of gas metered, standard conditions (m^3)

$$\text{Vmstd} = \frac{2.695 \text{ x Vm x (Pa + (DH/102)) x Yd}}{(\text{T + Tm})}$$

= 0.6349 m^3

Tm = 6 °C
Vm = 0.7151 m^3
Pa = 99.5 kPa
DH = 41.6 mm H_2O
Yd = 0.920

Moisture content

Bwo = Vwstd/(Vwstd +Vmstd)
= 0.0474

5.3 - Calculations Sample Run No. 1 Cont.

Dry total flow of stack gas, standard conditions (m^3/min)

$$Qstd = \frac{Q \times Ps(2.695)(1 - Bwo)}{Ts + 273}$$

$= 434$ m^3/min

Ts = 77.3 °C

Ps = 99.5 kPa

Percent isokinetic

$$\%I = \frac{(6.184 \times 10^5)(Ts + 273) \times Vmstd}{Ps \times V \times Aa \times t \times (1 - Bwo)}$$

= 102.8 %

Aa = 28.3 area of nozzle mm^2

Filter & rinsing weights sample no. 1

weight gain on filters =	23.88	mg
weight of acetone wash =		mg
total weight gain (M) =	23.88	mg

Particulate concentration (mg/m^3)

C = M/Vmstd

= 37.61 mg/m^3

M = 23.88 mg

Particulate emission rate (kg/hr)

E = (C x Qstd x 60)/1000000

= 0.98 kg/hr

5.4 - Calculations Sample Run No. 2

On-site measurements

O2 = 17.1 % CO2 = 2.0 % N2 = 80.9 %
Bws = 0.05 Ps = 99.5 kPa Ts = 349.0 K

Md = Molecular weight of gas at DGM (g/g mole)
Md = (0.44 x $\%CO_2$) + (0.32 x $\%O_2$) + (0.28 x $\%N_2$)
= 29.00 g/g mole

Ms = Molecular weight of gas wet (g/g mole)
= 28.48 g/g mole

Stack gas velocity at sample points

V = Kp x Cp x √(Ts.DP/Ps.Ms)
= 15.42 m/s

Kp = 4.07
DP = 117.3 av. Dp at sample plane
Cp = 1.00 pitot tube coefficient

Stack gas volume at sample points

Q = V x A x 60
= 588.5 m^3/min

A = 0.64 area of stack m^2

Volume of water vapour collected, standard conditions (m^3)

Vwstd = 0.00124 x Vlc
= 0.0321 m^3

Vlc = 26 ml

Volume of gas metered, standard conditions (m^3)

$$Vmstd = \frac{2.695 \times Vm \times (Pa + (DH/102)) \times Yd}{(T + Tm)}$$

= 0.6196 m^3

Tm = 7 °C
Vm = 0.7004 m^3
Pa = 99.5 kPa
DH = 41 mm H_2O
Yd = 0.920

Moisture content

Bwo = Vwstd/(Vwstd +Vmstd)
= 0.0493

5.4 - Calculations Sample Run No. 2 Cont.

Dry total flow of stack gas, standard conditions (m^3/min)

$$Qstd = \frac{Q \times Ps(2.695)(1 - Bwo)}{Ts + 273}$$

Ts = 76.0 °C

Ps = 99.5 kPa

= 430.0 m^3/min

Percent isokinetic

$$\%I = \frac{(6.184 \times 10^5)(Ts + 273) \times Vmstd}{Ps \times V \times Aa \times t \times (1-Bwo)}$$

Aa = 28.3 area of nozzle mm^2

= 101.3 %

Filter & rinsing weights sample no. 2

weight gain on filters =	20.55	mg
weight of acetone wash =		mg
total weight gain (M) =	20.55	mg

Particulate concentration (mg/m^3)

C = M/Vmstd

= 33.17 mg/m^3

M = 20.55 mg

Particulate emission rate (kg/hr)

E = (C x Qstd x 60)/1000000

= 0.86 kg/hr

5.5 - Sample Blank

An overall sample blank was taken after the measurement series, following the sampling procedure in the methodology without starting the suction device and keeping the blank in the duct for 15 minutes with the sampling nozzle 180o from the direction of flow. This leads to an estimation of the dispersion of results related to the whole procedure.

weight gain on filters = 0.00005 mg

weight of acetone wash = mg

total weight gain (M) = 0.00005 mg

Particulate concentration (mg/m^3)

C = M/Vmstd   M = 0.05 mg

= 0.08 mg/m^3

5.6 - Sampling Conditions

	Sample Run No. 1			Sample Run No. 2		
Sample Position	Stack Temp °C	Velocity Pressure DP (Pa)	Nozzle Area mm^2	Stack Temp °C	Velocity Pressure DP (Pa)	Nozzle Area mm^2
0.15D	78	117	28.3	76	115	28.3
0.85D	78	119	28.3	77	116	28.3
0.15D	76	119	28.3	76	117	28.3
0.85D	77	123	28.3	75	121	28.3

5.7 - Weighing Results

The below filters and acetone rinsing's were weighed on a balance in a temperature controlled room with corrections made for differences in atmospheric pressure. Control parts and blank filters are used to confirm accuracy of weighing's.

Sample Run No.1.	Ref No.	Weight gms			Sample time at each point (mins)	% weight gain
		Before	After	Collected		
Filter Acetone	25	0.05597	0.07985	0.02388	8.0	42.7%
			Total weight =	0.02388		
Sample Run No.2.	Ref No.	Weight gms			Sample time at each point (mins)	
		Before	After	Collected		
Filter Acetone	26	0.05609	0.07664	0.02055	8.0	36.6%
			Total weight =	0.02055		
Sample Blank	Ref No.	Weight gms			Sample time at each point (mins)	
		Before	After	Collected		
Filter Acetone	27	0.05586	0.05591	0.00005	n/a	0.1%
			Total weight =	0.00005		

6. Uncertainty calculation for EN 13284-1:2017

Sample Run No. 1

Limit value	50	**mg.m^{-3}**	O2 Ref	21	%
Measured conc.	37.61	**mg.m^{-3}**			

Measurement Equation

$$c = \frac{m}{V} f_c$$

Measured Quantities	**Symbol**	**Value**	**Standard uncertain**		**Units**	**Uncertainty %**		**Requirement of std**
Sampled Volume	V_m	0.7151	uV_m	0.001	**m^3**	0.14		<=2%
Sampled gas Tem	T_m	279.0	uTm	2	k	0.72		<=1%
Sampled gas Pressure	ρ_m	99.5	$u\rho_m$	0.5	**kPa**	0.50		<=1%
Sampled gas Humidity	H_m	4.74	uH_m	1	**% by vol**	0.21		<=1%
Oxygen content	$O_{2,m}$	17.9	$uO_{2,m}$	0.1	**% by vol**	0.56		<=5%
Mass particulate	m	23.88	um	0.01	**mg**	0	0.03	<5% of limit val
Note - Sampled gas humidity, temperature and pressure are values at the gas meter								
Leak	L	0.34			**%**	0.34		<=2%
Uncollected Mass	UCM	0.05			**mg**	0.21		<=10%
(In stack filter - no rinse)								

Intermediate calculations

Factor for std conds	fs	0.89					
uncertainty components	symbol	**sensitivity coeff**		**u (in units of fs)**			
	ρ_m	0.009		0.004			
	H_m	0.009		0.009			
	T_m	0.003		0.006			
	ufs			0.012			1.37
Corrected volume	V	0.63	uV	0.009	**m^3**	$V = V_m f_s$	1.38
Factor for O2 correction	fc	1.00					
uncertainty components	symbol	**sensitivity coeff**		**u**			
	$O_{2,m}$	0.32		0.032			
Factor for O2 Corr	ufc	1.00		0.032			1.00

$$f_s = \frac{(100 - H_m)}{100} \frac{273}{T_m} \frac{\rho_m}{101.3}$$

$$f_c = \frac{21 - O_{2,ref}}{21 - O_{2,m}}$$

Parameter	**Uncertainty**	**Value**	**Units**	**ens coeff**	**Uncertainty in Resul**		**Uncertainty as %**	
Volume(stp)	V	0.63	m^3	59.24	0.52	mg.m^{-3}	1.38	%
Mass	m	23.88	mg	1.58	0.02	mg.m^{-3}	0.04	
Factor for O2 Correction	fc	1.00		0.00	0.00	mg.m^{-3}	0.00	%
Leak	L	0.07	mg.m^{-3}	1.00	0.07	mg.m^{-3}		
Uncollected mass	UCM	0.03	mg	1.58	0.05	mg.m^{-3}		
Combined uncertainty					**0.52**	mg.m^{-3}		

Expanded uncertainty expressed with a level of confidence of 95% **2.79 %**

Expanded uncertainty expressed with a level of confidence of 95% **1.05 mg.m^{-3}**

6. Uncertainty calculation for EN 13284-1:2017

Sample Run No. 2

Limit value	50	**mg.m^{-3}**	O2 Ref	21	**%**
Measured conc.	33.17	**mg.m^{-3}**			

Measurement Equation

$$c = \frac{m}{V} f_c$$

Measured Quantities	**Symbol**	**Value**	**Standard uncertain**		**Units**	**Uncertainty %**		**Requirement of std**
Sampled Volume	V_m	0.7004	uV_m	0.001	**m^3**	0.14		<=2%
Sampled gas Tem	T_m	280.0	uTm	2	k	0.71		<=1%
Sampled gas Pressure	ρ_m	99.5	$u\rho_m$	0.5	**kPa**	0.50		<=1%
Sampled gas Humidity	H_m	4.93	uH_m	1	**% by vol**	0.20		<=1%
Oxygen content	$O_{2,m}$	17.1	$uO_{2,m}$	0.1	**% by vol**	0.58		<=5%
Mass particulate	m	20.55	um	0.01	**mg**	0	0.03	<5% of limit val
Note - Sampled gas humidity, temperature and pressure are values at the gas meter								
Leak	L	0.38			**%**	0.38		<=2%
Uncollected Mass	UCM	0.05			**mg**	0.24		<=10%
(In stack filter - no rinse)								

Intermediate calculations

$$f_s = \frac{(100 - H_m)}{100} \frac{273}{T_m} \frac{\rho_m}{101.3}$$

Factor for std conds	fs	0.88					
uncertainty components	symbol	**sensitivity coeff**		**u (in units of fs)**			
	ρ_m	0.009		0.004			
	H_m	0.009		0.009			
	T_m	0.003		0.006			
	ufs			0.012			1.37
Corrected volume	V	0.62	uV	0.009	m^3	$V = V_m f_s$	1.38
Factor for O2 correction	fc	1.00					
uncertainty components	symbol	**sensitivity coeff**		**u**			
	$O_{2,m}$	0.26		0.026			
Factor for O2 Corr	ufc	1.00		0.026			1.00

$$f_c = \frac{21 - O_{2,ref}}{21 - O_{2,m}}$$

Parameter	**Uncertainty**	**Value**	**Units**	**ens coeff**	**Uncertainty in Resul**		**Uncertainty as %**	
Volume(stp)	V	0.62	m^3	53.53	0.46	mg.m^{-3}	1.38	%
Mass	m	20.55	mg	1.61	0.02	mg.m^{-3}	0.05	
Factor for O2 Correction	fc	1.00		0.00	0.00	mg.m^{-3}	0.00	%
Leak	L	0.07	mg.m^{-3}	1.00	0.07	mg.m^{-3}		
Uncollected mass	UCM	0.00	mg	1.61	0.00	mg.m^{-3}		
Combined uncertainty					**0.46**	mg.m^{-3}		

Expanded uncertainty expressed with a level of confidence of 95% **2.79 %**

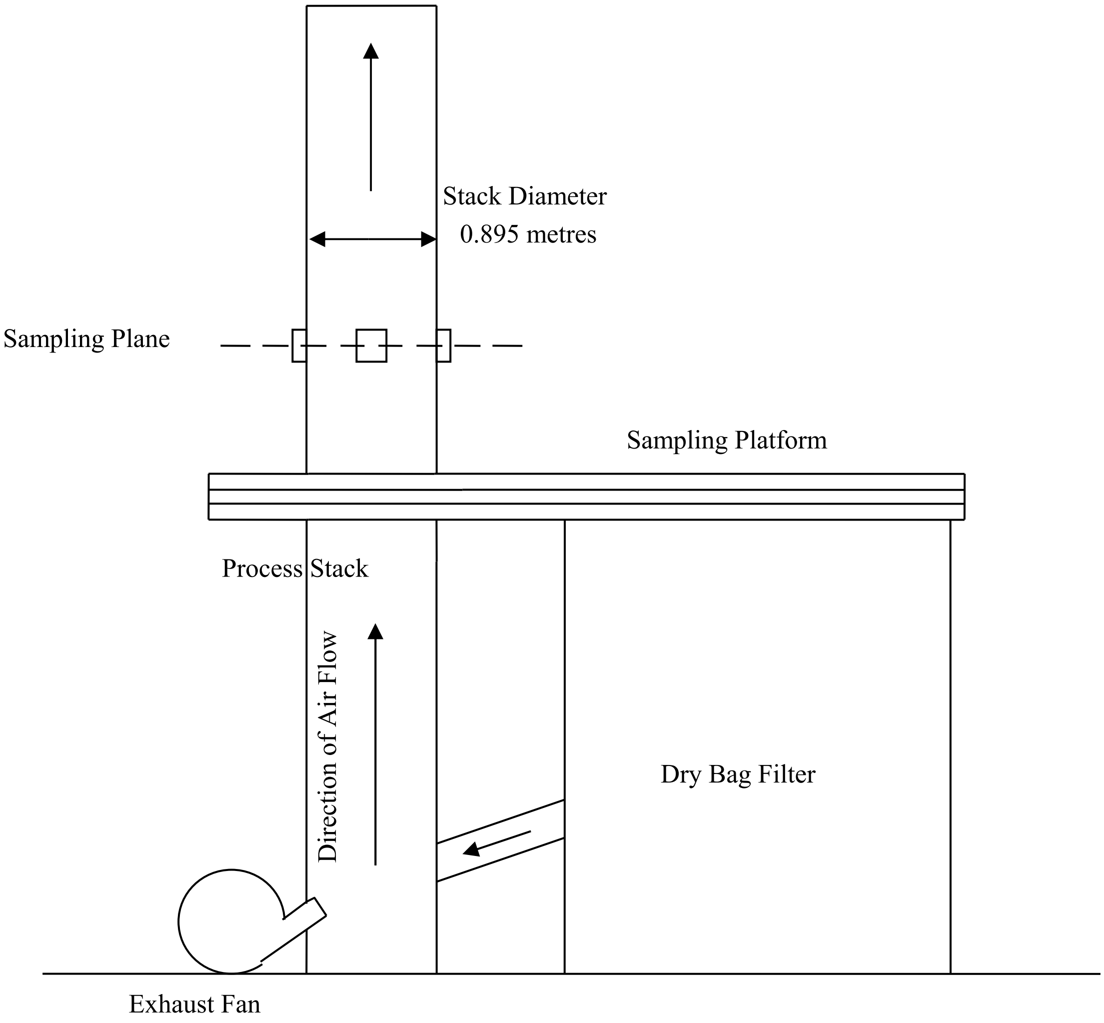
Expanded uncertainty expressed with a level of confidence of 95% **0.93 mg.m^{-3}**

APPENDICES

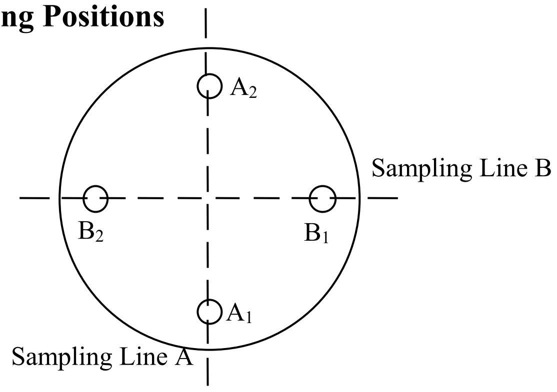
Appendix 1

Sampling Location Plan

A.1 Process Plant Layout



A.2 Sampling Positions



Appendix 2

Sampling Location Image