

# Report for the Periodic Monitoring of Emissions to Air

## Part 1. Executive summary

**Permit Number:** PPC/156

**Operator:** Meggit Aircraft Braking

**Installation:** Coventry Plant

**Monitoring Date:** 23 February 2009

**E.E. Report Ref.:** 38279

**Client Name:** Meggit Aircraft Braking

**Client Address:** Holbrook Lane  
Coventry  
CV6 4AA

**Monitoring Organisation:** Environmental Evaluation Ltd. (Head Office)  
Lawton Square  
Delph  
Oldham  
OL3 5DT

**Date of Report:** 18 March 2009


**Report Written by:** D Shields

**Function:** Team Leader

**Report Approved By:** T Ledwith

**MCERTS Registration No.:** MM 03 425

**Technical Endorsements:** TE1, TE2, TE3, TE4

**Signed:** 

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# 1 Part 1: Executive Summary

## 1.1 Monitoring Objectives

Meggit Aircraft Braking has been authorised under the Environmental Protection Act and associated legislation to operate various processes at their Coventry Plant site, and a condition of that authorisation is that emission monitoring is undertaken on a regular basis to prove compliance or otherwise against prescribed emission limit values.

This report details the testing undertaken in: February 2009

The substance monitoring requirements for each emission point are detailed below.

Substances to be monitored	Emission Point Identification
	<i>Main Stack</i>
Flow	✓
Temperature	✓
Fluorides	✓
Water vapour	✓

**1.2 Monitoring Results**

Emission Point	Substance to be Monitored	Emission Limit Value	Periodic Monitoring Result	Uncertainty	Units	Reference Conditions	Date of Monitoring	Start and End Times	Monitoring Method Reference	Accreditation for use of Method	Operating Status
Main Stack	Fluorides	5	0.01	± 0.002	mgm <sup>-3</sup>	273K and 101.3 kPa at 20.9% Oxygen Wet Basis	23/02/2009	10:07 - 12:07	BS ISO 15713:2006	None	Normal

**1.3 Operating Information**

Emission Point Reference	Date	Process Type	Process Duration	Feedstock	Abatement
Main Stack	23 February 2009	Batch	Batch	Brake components	Scrubber

**1.4 Monitoring Deviations**

Emission Point Reference	Substance Deviations	Monitoring Deviations	Other Relevant Issues
Main Stack	None	None	None

# Report for the Periodic Monitoring of Emissions to Air

## Part 2. Supporting Information

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**Operator:** Meggit Aircraft Braking

**Installation:** Coventry Plant

**Monitoring Date:** 23 February 2009

**E.E. Report Ref.:** 38279

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**Signed:** \_\_\_\_\_

## APPENDICES

### Appendix A: General Information

#### A1. Environmental Evaluation Limited Staff Details

Team Leader: D Shields  
MCERTS No. MM 02 051  
Certification Level: MCERTS Level 2  
Technical Endorsements: TE1, TE2, TE3, TE4

Site Technician: S White  
MCERTS No. MM 06 776  
Certification Level: MCERTS Level 1  
Technical Endorsements: TE1

#### A2. Environmental Evaluation Limited Method Details

The indicated substances were measured by the standards and in house methods specified in the table below:

Substance	Standard	EE. Reference
Flow	BS EN 13284:2001	EE/P/002 & 2a
Temperature	BS EN 13284:2001	EE/P/002 & 2a
Fluorides	BS ISO 15713:2006	EE/P/017
Water vapour	BS EN 14790:2005	EE/P/013

#### A3. Sub-Contract

Analysis was subcontracted to a UKAS accredited laboratory.

#### A4. Equipment Used in the Monitoring Campaign

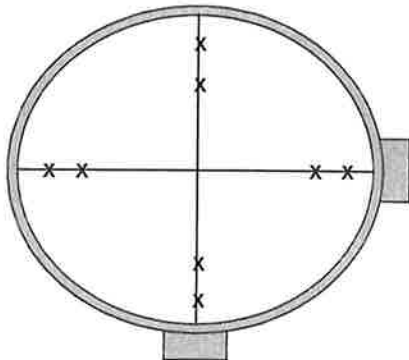
Equipment checklists appropriate to the methods were used.

Equipment Type	EE Equipment Reference Code
Unit	LCL 8, 24 and 13
Pitot	LCL 38
Manometer	LCL 26
Thermosensor	LCL 15
Thermocouple	LCL17
Tape Measure	LCL 18
Barometer	LCL 23
Probe	LCL 40, 30, 39
Nozzle	LCL 29
Vernier Callipers	LCL 14
stop watch	LCL 25

## Appendix B: Emission Information

### B1 - Main Stack Information

#### B1.1 Diagrams Showing the Dimensions and Monitoring Facilities of Main Stack

Photograph of Monitoring Point	Schematic of Sample Plane
No Photograph Available	

#### B1.2 Velocity and Temperature Measurement of Main Stack

Traverse Point	Sample Line A			Sample Line B			Sample Line C			Sample line D		
	Stack Temp. (°C)	ΔP (mmH <sub>2</sub> O)	Swirl (<15°)	Stack Temp. (°C)	ΔP (mmH <sub>2</sub> O)	Swirl (<15°)	Stack Temp. (°C)	ΔP (mmH <sub>2</sub> O)	Swirl (<15°)	Stack Temp. (°C)	ΔP (mmH <sub>2</sub> O)	Swirl (<15°)
1	22	5.5	Yes	22	5.5	Yes						
2	22	6	Yes	22	6	Yes						
3	23	6.5	Yes	23	6.5	Yes						
4	22	5.5	Yes	22	6.5	Yes						
5	22	6	Yes	22	5	Yes						
6	23	6	Yes	23	5.5	Yes						
7	22	5.5	Yes	22	6	Yes						
8	22	5.5	Yes	22	6.5	Yes						
9	22	5.5	Yes	22	6.5	Yes						
10	22	6	Yes	22	6	Yes						
	ΣΔP <sub>A</sub>	58		ΣΔP <sub>B</sub>	60		ΣΔP <sub>C</sub>			ΣΔP <sub>D</sub>		

Barometric Pressure (mmHg)	764	Port Depth (mm)	50
Static Pressure (mmH <sub>2</sub> O)	1.5	Port Seal Adaptor Depth (mm)	110
Diameter (m)	1.60	Assumed CO <sub>2</sub> (%)	0.0
---		Assumed O <sub>2</sub> (%)	20.9
Stack Area (m <sup>2</sup> )	2.011	Assumed CO (%)	0.0
Port Size (mm)	100	Assumed H <sub>2</sub> O (%)	5.0

**Appendix B1.3 - Site Measurements - Main Stack**

Company	Meggit Aircraft Braking	Test Conducted by	D Shields & S White
Site	Coventry Plant	Date of Test	23/02/2009
Plant Identification	Main Stack	Run Number	1

**Water Vapour Measurements**

Impinger	Initial Wt (g)	Final Wt (g)
1	712.4	715.9
2	795.5	803.6
3	662.4	662.4
4	879.3	886.9
5		
6		
7		

**Sample Reference Information**

Filter Ref.	DGM	DGM Temp (°C)
Probe Wash Ref.		
Blank Filter Ref.		
Blank Probe Wash Ref.		
Solution A Ref.	38279/S1/230209	
Solution B Ref.	38279/S2/230209	
Solution C Ref.		
Blank Solution Ref.	38279/S3/230209	

**Leak Test Results**

Initial Leak Test (%)	0.00000
Test Vacuum (mmHg)	15
Final Leak Test (%)	0.10000
Test Vacuum (mmHg)	15

**Sampling Measurements**

Point	Start and End Times	Duration (Min)	Vac (mmHg)	Stack Temp (°C)	Velocity Head ΔP (mmH2O)	√ΔP (√mm.H2O)	ΔP Orifice Meter (mm H2O)	DGM (litres)	DGM Temp (°C)		Temp (°C)				
									In	Out	Probe	Filter	Impinger	Resin	
1	10:07	10	7	22	5.5	2.35	24.80	747.7	14	14	160	160	5	---	
2		10	7	22	6	2.45	27.05	905	14	15	161	162	6	---	
3		10	7	23	5.5	2.35	24.80	1059	15	15	162	162	6	---	
4		10	7	23	5.5	2.35	24.80	1221	15	16	161	162	6	---	
5		10	7	22	6	2.45	27.05	1388	15	15	162	162	6	---	
6	12:07	10	7	23	5.5	2.35	24.80	1478	16	16	161	162	7	---	
7								1612.4							
8															
9															
10															
11															
12															
13															
14															
15															
16															
17															
18															
19															
20	120	60	7.00	22.50	5.67	2.38	25.55	864.70	14.83	15.17	161.17	161.67	6.00		



**Appendix B1. - Gaseous Fluorides to BS ISO 15713 - Main Stack**

<b>Company</b>	Meggit Aircraft Braking	<b>Test Conducted by</b>	D Shields & S White		
<b>Site</b>	Coventry Plant	<b>Date of Test</b>	23 February 2009		
<b>Plant Identification</b>	Main Stack				
<b>Volume of Water Vapour at Standard Conditions <math>V_{wstd}</math></b>					
$V_{wstd} = (0.00124) \times V_{lc}$	=	Blank	Test 1		Units $m^3$
		0.0238	0.0238		
Where:					
Constant	=	0.00124	0.00124		
$V_{lc}$ is the mass of water collected	=	19.2	19.2		mg
<b>Volume of Gas Metered, Standard Conditions <math>V_{mstd}</math></b>					
$V_{mstd} = \frac{(0.3592) \times V_m \times \left(P_b + \frac{\Delta H}{13.6}\right) \times Y_d}{(273 + T_m)}$	=	Blank	Test 1		Units $m^3$
		0.8855	0.8855		
Where:					
Correction for standard temperature and pressure	=	0.3592	0.3592		Kmm.Hg <sup>-1</sup>
$V_m$ is the volume metered	=	0.8647	0.8647		$m^3$
$P_b$ is the barometric pressure	=	764	764		mm.Hg
$\Delta H_{ave}$ is the average meter flow	=	25.6	25.6		mm.H <sub>2</sub> O
conversion from mm.H <sub>2</sub> O to mm.Hg	=	13.6	13.6		
$Y_d$ is the meter correction factor	=	1.0720	1.0720		
$^{\circ}C$ to K conversion constant	=	273	273		K
$T_m$ is the meter temperature	=	15.0	15.0		$^{\circ}C$
<b>Moisture Content <math>B_{wo}</math></b>					
$B_{wo} = \frac{V_{wstd}}{V_{mstd} + V_{wstd}}$	=	Blank	Test 1		
		0.026	0.026		
Where:					
$V_{wstd}$ is the volume of water vapour at standard conditions	=	0.0238	0.0238		$m^3$
$V_{mstd}$ is the volume of gas metered, standard conditions	=	0.8855	0.8855		$m^3$
<b>Velocity of Stack Gases <math>V_s</math></b>					
$V_s = K_p \times C_p \times \sqrt{\Delta P} \times \frac{\sqrt{(T_s) + 273}}{\sqrt{M_s \times P_s}}$	=	Blank	Test 1		$ms^{-1}$
		9.5	9.5		
Where:					
$K_p$ is the pitot tube velocity constant	=	34.97	34.97		
$C_p$ is the pitot coefficient	=	0.98	0.98		
$(\sqrt{\Delta P})_{ave}$ is the average square root of velocity heads	=	2.38	2.38		$\sqrt{mm.H_2O}$
$T_s$ is the stack temperature	=	22.5	22.5		$^{\circ}C$
$^{\circ}C$ to K conversion constant	=	273	273		K
$M_s$ is the molecular weight of gas	=	28.29	28.29		g/g mole
$P_s$ is the absolute pressure of stack gas	=	764	764		mm.Hg

**Appendix B1. - Gaseous Fluorides to BS ISO 15713 - Main Stack**

Actual Flow Rate of Stack Gases $Q_a$					
$Q_a = 60 \times A_s \times V_s$	=	Blank 1150.3	Test 1 1150.3		$m^3 \text{ min}^{-1}$
Where:					
Second to minute conversion	=	60	60		
$A_s$ is the cross-sectional area of stack	=	2.011	2.011		$m^2$
$V_s$ is the velocity of stack gases	=	9.5	9.5		$ms^{-1}$
Dry Total Flow Rate of Stack Gas $Q_{std}$					
$Q_{std} = \frac{Q_a \times P_s \times 0.3592 \times (1 - B_{wo})}{(\overline{T_s}) + 273}$	=	Blank 1040.5	Test 1 1040.5		$m^3 \text{ min}^{-1}$
Where:					
$Q_a$ is the actual flow rate of stack gases	=	1150.3	1150.3		$m^3 \text{ min}^{-1}$
$P_s$ is the absolute pressure of stack gas	=	764	764		mm.Hg
Correction for standard temperature and pressure	=	0.3592	0.3592		Kmm.Hg <sup>-1</sup>
$B_{wo}$ is the moisture content	=	0.026	0.026		
$T_s$ is the stack temperature	=	22.5	22.5		°C
°C to K conversion constant	=	273	273		K
$V_s$ is the velocity of stack gases	=	9.5	9.5		$ms^{-1}$
Percent Isokineticity %I					
$\%I = \frac{(4.6398 \times 10^6) \times (\overline{T_s} + 273) \times V_{mstd}}{P_s \times V_s \times A_n \times \theta \times (1 - B_{wo})}$	=	Blank 99.9	Test 1 99.9		%
Where:					
Constant	=	4.6398E+06	4.6398E+06		
$T_s$ is the stack temperature	=	22.5	22.5		°C
°C to K conversion constant	=	273	273		K
$V_{mstd}$ is the volume of gas metered, standard conditions	=	0.8855	0.8855		$m^3$
$P_s$ is the absolute pressure of stack gas	=	764	764		mm.Hg
$V_s$ is the velocity of stack gases	=	9.5	9.5		$ms^{-1}$
$A_n$ is the cross-sectional area of nozzle	=	28.56	28.56		$mm^2$
$\theta$ is the duration of test	=	60	60		minutes
$B_{wo}$ is the moisture content	=	0.026	0.026		
Particulate Concentration $C_{mgm^{-3}}$ - Dry Basis					
$C_{mgm^{-3}} = \frac{M_n}{V_{mstd}}$	=	Blank 0.007	Test 1 0.015		$mgm^{-3}$
Where:					
Reference number		38279/S3/2 30209	38279/S1/2 30209		
Mn1 - Fluoride mass in the first impinger.	=	0.006	0.01295		mg
Reference number			38279/S2/2 30209		
Mn2 - Fluoride mass in second impinger.	=	0	<0.005		mg
$V_{mstd}$ is the volume of gas metered, standard conditions	=	0.8855	0.8855		$m^3$

**Appendix B1. - Gaseous Fluorides to BS ISO 15713 - Main Stack**

Particulate Concentration $C_{mgm^{-3}}$ - Wet Basis					
$C_{mgm^{-3}(wet)} = C_{mgm^{-3}} \times \frac{(100 - Wv)}{100}$	=	Blank	Test 1		$mgm^{-3}$
		0.0	0.0		
Where					
Concentrations at 273k and 101.3kPa Dry Basis	=	0.0	0.0		$mgm^{-3}$
Wv is the water vapour content %	=	2.6	2.6		%
Particulate Concentration Corrected to 20.9 % Oxygen, Wet Basis					
$C_{atx\%} = C_{mgm^{-3}} \times \frac{20.9 - O_{2ref}}{20.9 - O_{2meas}}$	=	Blank	Test 1		$mgm^{-3}$
		0.0	0.0		
Where:					
Atmospheric oxygen concentration	=	20.9	20.9		%
$O_{2ref}$ is the reference oxygen concentration	=	20.9	20.9		%
$O_{2meas}$ is the measured oxygen concentration	=	*	*		%
* Oxygen Not Measured					
Particulate Emission Rate $E_{ghr^{-1}}$					
$E_{ghr^{-1}} = C \times Q_{std} \times \frac{60}{1000}$	=	Blank	Test 1		$ghr^{-1}$
		0	1		
Where:					
$C_{mgm^{-3}}$ is the Fluoride concentration, dry basis	=	0.0	0.0		$mgm^{-3}$
$Q_{std}$ is the dry total flow rate of stack gas	=	1040.5	1040.5		$m^3 min^{-1}$
60/1000 Conversion factor	=	0.060	0.060		
Comments on Compliance with BS ISO 15713					
Temperature maintained above 160°C				Pass	
Isokinetic Rate 95% to 115%				Pass	
Leak Rate <2%				Pass	
Overall Blank Value <10% of the LV <sup>a</sup>				Pass	
Duct gas flow with regard to stack axis <15°				Pass	
Duct gas flow: negative velocity - not permitted				Pass	
Duct gas flow: differential pressure at the pitot tube >5pa				Pass	
Duct gas flow: ratio of max to min velocity <3:1				Pass	
<p>Were all of the requirements of BS ISO 15713 fulfilled during the test?</p> <p style="text-align: center;"> <input checked="" type="checkbox"/> Yes      <input type="checkbox"/> No                 </p>					

**Appendix B1. - Gaseous Fluorides to BS ISO 15713 - Main Stack**

<b>Uncertainty Calculations</b>						
<b>Measurement Data</b>						
Measured Quantities	Symbol	Value	Standard Uncertainty		Units	
Sampled Volume	$V_m$	0.8855	(1%) $uV_m$	0.00885	$m^3$	
Sampled Gas Temperature	$T_m$	288.0	$uT_m$	3	k	
Sampled Gas Pressure	$p_m$	102.1	$up_m$	0.1	kPa	
Sampled Gas Humidity	$H_m$	2.6	$uH_m$	0.1	% by volume	
Oxygen Content	$O_{2,m}$	*	$uO_{2,m}$	0.01	% by volume	
MassFluoride	m	0.01	$um_m$	0.00	mg	
Leak	L	2	%	0.02	%	
Uncollected Mass	UCM	0			mg	
<b>Intermediate Calculation to Correct for Standardisation of Conditions</b>						
Factor for Std Conditions	fs	0.93				
Uncertainty Components	symbol	Sensitivity Coefficient		u (in units of fs)		
	$p_m$	0.009		0.001		
	$H_m$	0.010		0.001		
	$T_m$	0.003		0.010		
	ufs			0.010		
Corrected Volume	V	0.82	$uV$	0.012	$m^3$	
<b>Intermediate Calculation to Correct for Oxygen Correction</b>						
Factor for O <sub>2</sub> Correction	fc	1.00				
Uncertainty Components	symbol	Sensitivity Coefficient		u (in units of fc)		
	$O_{2,m}$	1.00		0.010		
Factor for O <sub>2</sub> Correction	ufc	1.00		0.010	%	
<b>Calculation of Expanded Uncertainty</b>						
Parameter		Value	Units	Sensitivity Coefficient	Uncertainty in Result	
Volume (Std conditions)	V	0.82	$m^3$	0.02	0.00	$mg.m^{-3}$
Mass	m	0.01	mg	1.10	0.00	$mg.m^{-3}$
Factor for O <sub>2</sub> Correction	fc	1.00		0.01	0.00	$mg.m^{-3}$
Leak	L	0.00	$mg.m^{-3}$	1.00	0.00	$mg.m^{-3}$
Uncollected mass	UCM	0.00	mg	1.10	0.00	$mg.m^{-3}$
Combined uncertainty					0.00	$mg.m^{-3}$
<b>Expanded Uncertainty K=2</b>					<b>10.88</b>	<b>%</b>
<b>Expanded Uncertainty K=2</b>					<b>0.002</b>	<b><math>mg.m^{-3}</math></b>

## Test Certificates

**RPS** Laboratories



**Test Certificate**

Date 10/03/2009

<b>Client</b>	Environmental Evaluation Ltd Lawton Square Delph Oldham Lancs OL3 5DT	<b>Order No.</b>	38279
		<b>Certificate No.</b>	WK09-1528
		<b>Issue No.</b>	1

<b>Contact</b>	Dan Shields	<b>Date Received</b>	02/03/2009
<b>Description</b>	3 solutions for HF	<b>Technique</b>	Ion Chromatography

<b>Sample No.</b>	<b>538479</b>	<b>38279/S1/230209</b>	<b>Method</b>
<b>Hydrofluoric acid</b>	0.07 µg/ml	185 ml	C27(U)

<b>Sample No.</b>	<b>538480</b>	<b>38279/S2/230209</b>	<b>Method</b>
<b>Hydrofluoric acid</b>	<0.05 µg/ml	100 ml	C27(U)

<b>Sample No.</b>	<b>538481</b>	<b>38279/S3/230209</b>	<b>Method</b>
<b>Hydrofluoric acid</b>	<0.05 µg/ml	120 ml	C27(U)

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### Test Certificate

Date 10/03/2009

<b>Client</b>	Environmental Evaluation Ltd	<b>Certificate No.</b>	WK09-1528
		<b>Issue No.</b>	1

**Tested By** Paul Robertson **Date** 09/03/2009

**Approved By** [Redacted] **Date** 10/03/2009

Andrew Chalmers  
Senior Chemist

For and on authority of RPS Laboratories Ltd.  
Standard terms and conditions are applicable, a copy is available on request.

**Method Symbols** (U) Analysis is UKAS Accredited  
(N) Analysis is not UKAS Accredited  
(S) Analysis is Subcontracted

Concentration values (mg/m3 and ppm) are provided to assist with interpretation only, they are not covered by the scope of UKAS accreditation

Analysis carried out on samples 'as received'

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**End of Report**